# REMOVAL OF HUMIC ACID FROM WATER USING AN OZONATION ALONE AND COMBINATION OF OZONATION AND ADSORPTION

DHIWYA A/P PARAMASIVAM

**UNIVERSITI SAINS MALAYSIA** 

2022

# REMOVAL OF HUMIC ACID FROM WATER USING AN OZONATION ALONE AND COMBINATION OF OZONATION AND ADSORPTION

by

# DHIWYA A/P PARAMASIVAM

Thesis submitted partial fulfilment of the requirement for the degree of Bachelor of

**Chemical Engineering** 

**June 2022** 

#### ACKNOWLEDGEMENT

First and foremost, I would like to express my deepest gratitude to the School of Chemical Engineering, Universiti Sains Malaysia for providing me this opportunity and medium to learn and enhance my knowledge and skills to be chemical engineer for the future. Secondly, I would like to thank Professor Dr. Ahmad Zuhairi Abdullah, my supervisor for Final Year Project, who has been very patient and supportive towards me in giving guidance and building criticism. Next, wholehearted thank you to Universiti Sains Malaysia (USM), specifically to the School of Chemical engineering in providing needed facilities for the research, required engineering knowledge and skills to be applied in the project. Sincere thanks to all the lecturers who conducted seminars and prepared us to complete the progress report. I would like to us this opportunity to thank my family for their prayers, support, and encouragement to complete the progress report successfully. Not forgetting to all my friends and all the people who have helped, supported and contributed to complete this report Finally, I would love to reach out and thank those who directly or indirectly, have lent their hand in completing this progress report.

# TABLE OF CONTENTS

ACKNOWLEDGEMENT
TABLE OF CONTENTS4
LIST OF TABLES
LIST OF FIGURES
LIST OF ABBREVIATION11
LIST OF SYMBOLS
ABSTRAK
ABSTRACT15
CHAPTER 1 INTRODUCTION16
<b>1.0 Introduction</b>
1.1 Background of Study16
1.1.1 Aquaculture
1.1.2 Global Demand for Aquaculture17
1.1.3 Aquaculture Wastewater
1.1.4 Humic Acid in Wastewater20
1.1.5 Wastewater Treatment
1.1.6     Advance Oxidation Process
1.2 Problem Statement

1.3	Objectives25
1.4	Sustainability of Wastewater Treatment26
СНА	PTER 2 LITERATURE REVIEW27
2.1	Aquaculture Wastewater27
2.2	Wastewater Treatment27
2.3	Limitation in Coagulation, Membrane Filtration, Anaerobic Digestion to Remove
Hum	ic Acid
2.3.1	Coagulation
2.3.2	Membrane Filtration32
2.3.3	Anaerobic Digestion
2.4	Advance Oxidation Process
2.5	Ozonation
2.6	Ozonation of Organic Compounds40
2.7	Ozonation Coupled with Adsorption42
СНА	PTER 3 METHODOLOGY46
3.1	Introduction
3.2	Materials and Chemicals Required48
3.3	Equipment and Facilities Required50
3.4	Experimental Set-Up
3.5	Humic Acid Solution Preparation52

3.6	Calibration of Humic Acid Concentration53
3.7	Experimental Procedure
3.7.1	Ozonation
3.7.1	(a) Effect of the concentration on humic acid degradation efficiency54
3.7.1	(b) Effect of pH on humic acid degradation efficiency55
3.7.2	Ozonation coupled with adsorption55
3.8	Data Analysis56
3.8.1	Kinetic Modelling56
3.8.2	Degradation Profile
СНА	PTER 4
RES	ULTS AND DISCUSSION
4.1	Introduction
4.2	2 FTIR Spectrum of Humic Acid58
4.3	Kinetics of Humic acid Degradation59
4.4	Effect of Humic Acid Concentration on Degradation Efficiency61
4.5	Effect of the pH on Humic Acid Degradation Efficiency63
4.6	<b>Effect of Catalytic Ozonation on Degradation Efficiency of ozonation66</b>
4.7	The effect of lava rocks with ozonation on the degradation efficiency of humic acid
4.8	Characterization of activated carbon72
4.9	Characterization of lava rocks74
4.1	0 Energy consumption of ozonation and catalytic ozonation

4.11 Sustainability	77
CHAPTER 5	78
CONCLUSION AND RECOMMENDATION	78
5.1 Conclusion	78
5.2 Recommendations for Future Research	79
REFERENCES	80
APPENDICES	

# LIST OF TABLES

<b>Table 1.1</b> Projection of fish production to 2030 under baseline scenario (Msangi et al., 2013)18
<b>Table 1.2</b> Elemental composition (weight%) and functional group content(mequ/g) in humic       acid. (Sharma et al., 2016)
<b>Table 2.1</b> Projects the classification of disinfection by-products and the health effects (Zazouli and Kalankesh, 2017)
<b>Table 2.2</b> Shows oxidation potential for some common oxidants (Huling and Bruce, 2006)36
<b>Table 2.3</b> Physical and chemical properties of ozone (Wei et al., 2017)
<b>Table 3.1</b> List of materials and chemicals
<b>Table 3.2</b> Chemical structure and relevant data for humic acid
<b>Table 3.3</b> List of equipment and facilities  50
<b>Table 3.4</b> Tabulated data of the various humic acid concentrations with absorbance detected by UV-Vis Spectrophotometer
<b>Table 4.1</b> Non-linear pseudo first order kinetic constant
<b>Table 4.2</b> Physico-chemical characteristics of activated carbon
<b>Table 4.3</b> Physico-chemical characteristics of lava rocks as affected by ozone oxidation

# LIST OF FIGURES

Figure 1.1 World aquaculture and capture fisheries (OECD-FAO Agricultural Outlook 2020-2029, 2021).       18
Figure 2.1 Classification of wastewater treatment (Shindhal et al., 2020)
<b>Figure 2.2</b> Schematic illustration of fluorescence spectra (dotted lines) and location of EEM pekas (Ellipse) in NOM (Chen et al., 2018)
<b>Figure 2.3</b> Shows classification of advance oxidation process (Divyapriya et al., 2016)37
Figure 2.4 Shows dipolar cyclo addition of ozone (Lenntech.com, 2021)
Figure 3.1 Overall experiment flow chart
Figure 3.2 Scheme of experimental set-up
Figure 3.3 Calibration curve of humic acid concentration in UV-Vis in Spectrophotometer54
Figure 4.1 FTIR spectrum of humic acid
Figure 4.2 Non-linear fit of pseudo first order kinetic model
<b>Figure 4.3</b> Degradation efficiency of humic acid for 2 hours at different concentration63
Figure 4.4 Degradation efficiency of humic acid for 2 hours at different pH
Figure 4.5 Effect of catalytic ozonation on the removal efficiency of humic acid
Figure 4.6 Difference between ozonation and catalytic ozonation
<b>Figure 4.7</b> The effect of lava rocks on the removal efficiency of humic acid71
Figure 4.8 Isotherm linear plot of activated carbon  72

Figure 4.9 (a) Initial stage of activated carbon and Figure 4.9 (b) Final stage of activated ca	
Figure 4.10 The operation energy required for ozonation and catalytic ozonation	76
Figure 4.11 Persian Shield Plants	77

# LIST OF ABBREVIATION

AC	Activated Carbon	
AOP	Advance Oxidation Process	
BOD	Biochemical Oxygen Demand	
CHBr <sub>3</sub>	Bromoform	
CHBrCl <sub>2</sub>	Bromodichloromethane	
CHCl <sub>3</sub>	Chloroform	
COD	Chemical Oxygen Demand	
DBP	Disinfection By-Product	
DOC	Dissolved Organic Carbon	
e	electron	
E. Coli	Escherichia coli	
Eh	Oxidation Potential	
EPS	Extracellular Polymeric Substances	
Fe <sup>3+</sup>	Iron (III)	
$\mathrm{H}^+$	Hydrogen ion	
$H_2O_2$	Hydrogen Peroxide	
HA	Humic Acid	
HAA	Haloacetic acid	
HO <sub>2</sub>	Water	
HO2 <sup>-</sup>	Hydroperoxyl	
HOCl	Hypochlorous Acid	
HS	Humic Substances	
$HS0_{5}^{-}$	Peroxymonosulfate anion	

$MnO_4^-$	Permanganate ion
NOM	Natural Organic Matter
O2	Oxygen
O3	Ozone
OCl2	Dichlorine Monoxide
OH	Hydroxide
OH·	Hydroxyl radical
pH	Potential of Hydrogen
$S_2 O^{-2}$	Persulfate anion
SDG	Sustainability Development Goal
<i>S0</i> 4 <sup>.–</sup>	Sulfate radical
TOC	Total Organic Matter
THM	Trihalomethanes
TiO <sub>2</sub>	Titanium Dioxide
TOM	Total Organic Matter
TSS	Total Suspended Solid
UNICEF	United Nations Children's Fund
US	Ultrasonic sound
US EPA	United States Environmental Protection
	Agency
UV	Ultraviolet
UV/Vis	Ultraviolet Visible Light
V	Voltage
VSS	Volatile Suspended Solid
WHO	World Health Organization

# LIST OF SYMBOLS

$C_1$	initial concentration		
$C_2$	final concentration		
$C_{\mathrm{HA}_{\mathrm{e}}}$	final concentration of humic acid		
C <sub>HAO</sub>	initial concentration of humic acid		
Ci	initial concentration of treated pollutant		
Ce	effluent concentration of treated pollutant		
Co	initial humic acid concentration		
Ct	humic acid concentration at different time		
	interval		
$\mathbf{k}_1$	rate of constant of in the reaction of		
	ozonation		
V	volume of treated water		
$\mathbf{V}_1$	initial volume (stock volume)		
$V_2$	final volume		
W	power of oxidation system		

#### **REMOVAL OF**

# HUMIC ACID FROM WATER USING AN OZONATION ALONE AND COMBINATION OFOZONATION AND ADSORPTION

## ABSTRAK

Kajian ini menilai prestasi ozonasi sahaja dan proses ozonasi hibrid di mana ozonasi ditambah dengan karbon yang diaktifkan dan batu lava masing-masing. Penyingkiran asid humik dinilai oleh penyerapan UV254. Apabila ozonasi digunakan semata-mata, penyingkiran adalah 54.91% pada kepekatan asid humik 10 mg/L, pH 7 dan masa pengoksidaan 20 minit. Hasilnya menunjukkan bahawa penggunaan karbon diaktifkan sebagai penyerap meningkatkan penyingkiran asid humik berbanding dengan ozonasi sahaja kerana boleh bertindak sebagai penjerap dan pemangkin. Kecekapan penyingkiran adalah 96.36 % pada masa pengoksidaan 20 minit, pH 7 dan pemangkin pemangkin 1 g/L. Eksperimen pengoksidaan juga dijalankan menggunakan batuan lava dan kecekapan penyingkiran adalah 76.76 % pada masa pengoksidaan 20 minit, pH 7 dan pemuatan 5g/L. Ini menunjukkan bahawa ozonasi ditambah dengan karbon diaktifkan sangat berkesan berbanding dengan ozonasi sahaja.

## **REMOVAL OF**

# HUMIC ACID FROM WATER USING AN OZONATION ALONE AND COMBINATION OFOZONATION AND ADSORPTION

# ABSTRACT

This study evaluates the performance of ozonation alone and hybrid ozonation process in where ozonation coupled with activated carbon and lava rocks respectively. The removal of humic acid was evaluated by UV<sub>254</sub> absorbance. When ozonation was used alone, the removal was 54.91% at a humic acid concentration of 10 mg/L, pH 7 and oxidation time of 20 minutes. The results showed that the use of activated carbon as an adsorbent increased the removal of humic acid compared to ozonation alone as it can act as adsorbent and catalyst. The removal efficiency was 96.36 % at oxidation time of 20 minutes, pH 7 and catalyst loading of 1 g/L. The oxidation experiment was also carried out using lava rocks and the removal efficiency was 76.76 % at oxidation time of 20 minutes, pH 7 and loading of 5g/L. This indicates that ozonation coupled with activated carbon is highly effective compared to lava rocks. In conclusion, hybrid ozonation process yields better compared to ozonation alone.

## **CHAPTER 1**

## INTRODUCTION

# **1.0 Introduction**

This research analyses the efficiency of advanced oxidation processes to that of ozonation alone and the combination of ozonation and adsorption in degradation of humic acid. Humic acid will be modelled as a synthetic aquaculture wastewater. The primary objective of the experiment is to study removal efficiency of ozone under certain range of critical process variables with ozone alone and the combination of ozone and adsorption process. This investigation aids in the identification of a more effective humic acid breakdown approach in wastewater and promote global optimization of ozonation and adsorption as a humic acid wastewater treatment technique.

#### 1.1 Background of Study

# 1.1.1 Aquaculture

Aquaculture is commonly assumed to refer to the farming of aquatic species such as fish, mollusks, crustaceans, and aquatic plants. There are two types of aquacultures: intensive and extensive aquaculture (Lucas, 2019). Intensive aquaculture takes place in ponds, cages, and tanks, whereas extensive aquaculture takes place in the ocean, man-made lakes, and rivers. In intense aquaculture, nutrients are obtained through introduced feeds with no usage of natural diets, whereas in extensive aquaculture, nutrients are obtained from natural food organisms or waste. Aquaculture is expanding to grow at a faster rate, as animal nutrients becomes crucial for majority of human beings. Consuming fish becomes cornerstone of many people's cultural customs due to the essential nutrients that present inside it like calcium, omega-3 fatty acids, phosphorus and abundance of minerals. In addition, The American Heart Association said that eating fish at least twice a weak can prevent heart attack and stroke (Norton, 2018). In

conclusion, seafood production has reached its peak and eventually the demand for aquaculture raises as it becomes the source for seafood production.

# **1.1.2 Global Demand for Aquaculture**

In 2018, global aquaculture output reached another all-time high of 114.5 million tonnes of live weight and it consists of 82.1 million tonnes of aquatic animals, 32.4 million tonnes of algae and 26000 tonnes of ornamental seashells and pearls (Food and Agriculture Organization of United States, 2020). Out of 82.1 million tonnes of aquatic animals, the number of fish produced is more than half of the value which is 54.3 million tonnes. It can be clearly seen that; production of fish contributes more to the aquaculture sector economically. Aquaculture industries are attracted by the high demand of fish since 46% of total fish production is projected in 2018 with 52% of that value going to human consumption. The production of fish not necessarily used for human consumption but at the same time it will be used to make fish meal and fish oil. By 2029, aquaculture production is expected to reach 105Mt (OECD-FAO Agricultural Outlook 2020-2029, 2021). Based on (Global Newswire, 2021), the aquaculture market is expected to be worth \$2.7 billion by 2020 in United States while China, the world's second largest economy, is expected to reach a projected market size of US\$177.3 billion by 2027. Hence, aquaculture production expected to increase over the next decade. Figure 1.1 projects regarding the trends of world aquaculture and capture fisheries and Table 1.1 shows regarding the projection of fish production to 2030 under baseline scenario.

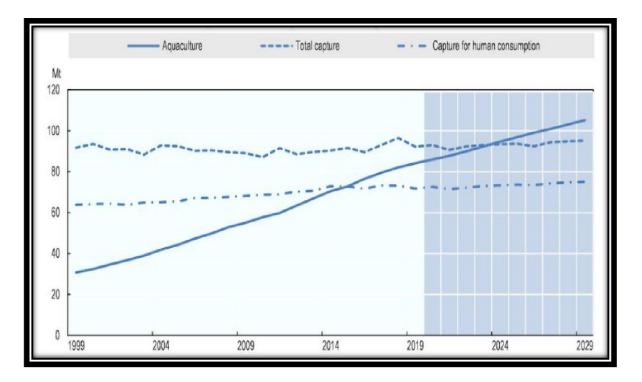


Figure 1.1 World aquaculture and capture fisheries (OECD-FAO Agricultural Outlook 2020-2029, 2021)

	2010-2030 increase	2010-2030 increase	Share of 2010-2030
	in production	in production (%)	increase coming
	(million tons)		from aquaculture (%)
Africa South of the	0.3	4	64
Sahara			
Middle East and	0.8	22	97
North Africa			
India	4.8	60	98
Other South Asia	2.4	32	82
Southeast Asia	7.9	38	97
Japan	0.5	-9	-

Table 1.1 Projection of fish production to 2030 under baseline scenario (Msangi et al., 2013)

China	16.5	31	101
Other East Asia and	0.3	7	105
Pacific			
Latin America and	2.1	11	94
Caribbean			
North America	0.2	4	103
Europe and Central	0.8	6	122
Asia			
Rest of the World	0	1	60
Global Total	35.7	24	100

# **1.1.3 Aquaculture Wastewater**

Aquaculture sector is growing rapidly to satisfy the current demand. Although it is growing intensively but it has harmed the environment in producing large number of wastewaters. Based on a study by shrimp aquaculture effluent consists of 87.74 mg/L of total organic matter, (TOM) which is hazardous to the environment and living organisms as well (Arfiati et al., 2021). Aquaculture wastewater can come from a nutrient, fertiliser, pesticide, or herbicide source, or it can come from a nutrient, fertiliser, pesticide, animals or plants. Therefore, organic material will be the pollutant in most of the case. The treated or untreated wastewater will be released to the surface waters. Organic pollutants play a prominent role in wastewater consists of high concentration of organic pollutants with high BOD and COD values. Natural Organic Matter, NOM consists of many functional groups. It is a heterogenous mixture of organic materials that present mostly in aquatic environment (Swietlik et al., 2004). However, humic and fulvic acid contributes more to the NOM (Kan et al., 2016). In conclusion,

wastewater treatment needs to be conducted to remove the natural organic pollutants present in the water. Wastewater treatment is critical since fresh water is scarce in some areas, and humans rely on treated wastewater for their everyday activities. According to the 2017 WHO and US EPA census, Australia, California, Texas, Singapore, Namibia, South Africa, Kuwait, Belgium, and the United Kingdom are among the states that reuse treated wastewater for drinking water production and distribution (Veolia, 2020). Hence, NOM must be removed from the aquaculture wastewaters which will be reused for other activities.

# 1.1.4 Humic Acid in Wastewater

Humic acid belongs to humus family in where it is produced from the decomposition of plants and animal residues. The chemical composition of humic acid varies depending on their geographic origin, age, climate, and biological circumstances. Hence, there is a range for their molecular in where it is in the range of 2.0 to 1300 kDa (de Melo et al., 2016). The elements involved are carbon, oxygen, nitrogen and sulphur. There are wide functional groups involved in the humic acid such as acid groups, carboxylic acids, phenolic OH, alcoholic OH, quinoide and methoxy OCH. Under acidic condition (pH<2), it is not soluble in water. Nevertheless, it is soluble at high pH conditions. Humic acid mostly present in the surface waters due to the wide range of functional groups. Based on Stevenson's hypothesis, polymerization reaction between phenolic, amine and aldehyde functional groups can form humic acid in natural water (Sharma et al., 2016). When humic acid is present in water, it affects the colour of the water. Moreover, it acts as a precursor for formation of trihalomethanes and for low and high molecular weight chlorine containing compounds during chlorination process (Suffet and Maccarthy, 1988.) Finally, humic acid causes mammalian cells to be carcinogenic which eventually leads to growth retardation. As a result, humic acid needs to be removed during the wastewater treatment. Table 1.2 below shows the elemental composition and functional group content in humic acid.

Elemental Composition (Weight %)	
С	53.6-58.7
Н	3.2-6.2
Ν	0.8-5.5
0	32.8-38.3
S	0.1-0.5
Functional Groups (mequ/g)	
Acid groups, total	5.6-8.9
Carboxylic acids	1.5-5.7
Phenolic OH	2.1-5.7
Alcoholic OH	0.2-4.9
Quinoide	0.1-5.6
Methoxy OCH <sub>3</sub>	0.3-0.8

Table 1.2 Elemental composition (weight%) and functional group content(mequ/g) in humic acid. (Sharma et al., 2016)

# **1.1.5 Wastewater Treatment**

Preliminary, primary, secondary, and tertiary treatment are the four stages of traditional wastewater treatment. Primary treatment removes settleable organic materials and inorganic solids after preliminary treatment removes coarse particulates found in wastewater. During secondary treatment, organic materials and suspended particles are removed even more thoroughly. Finally, tertiary treatment is used to eliminate pollutants that were not removed during secondary treatment and to disinfect the water (Gedda et al., 2021). The treated water from conventional treatment identified with contaminants as some compounds causes problems

while undergoing the wastewater treatment. Hence, new technologies are being implemented in wastewater treatment plant to produce high quality water.

# **1.1.6 Advance Oxidation Process**

Glaze et al introduced Advance Oxidation Process, (AOP) in 1987, and it is a preferred technology. To optimize the effluent treatment process, this technology is being introduced. To eliminate organic and inorganic contaminants, (AOP) uses strong oxidising agents or irradiation. The fundamental goal of (AOP) is to produce hydroxyl radicals that will oxidise the pollutants in the wastewater. When hydroxyl radicals react with organic matter, oxygenated molecules such as carbonyl compounds, organic acids, and alcohol are produced, whereas inorganic matter has electrons removed, resulting in a greater oxidation state. In conclusion, introduction (AOPs) such as ozonation is vital in decreasing humic acid in wastewater to prevent hazards to the aquatic environment and human health.

#### **1.2 Problem Statement**

Freshwater is essential for human health and social growth. There are approximately 332.5 million cubic miles of water on the planet, but only around 1% of it is readily available for home and commercial use as freshwater. Furthermore, only two-thirds of the available water is drinkable, with the remainder being unusable owing to pollution (Abdul Aziz and Abu Amr, 2019). 780 million people lack access to drinking water, according to WHO and UNICEF statistics, with 185 million relying on surface water to satisfy their daily requirements in certain developing countries, chemical pollution of surface waterways, mostly owing to industrial and aquaculture wastes, poses a considerable health danger. Natural organic matter, (NOM) plays a prominent role in wastewater. NOM concentrations in surface waters vary from 0.1 to 20 mg/L, with humic compounds such as humin, fulvic acid, and humic acid accounting for the majority. Humic acid (HA) is one of the most challenging NOM fractions to remove,

accounting for over 50–90% of total organic matter in surface water (Kan et al., 2016). Hence, humic acid is modelled to be the synthetic wastewater in this study.

The presence of humic acid in drinking water can give it an unappealing colour and flavour. Furthermore, during the disinfection process, the reaction of humic acid with chlorine produces disinfection by- products (DBPs). The main DPBs formed during the disinfection process are trihalomethanes (THM) and haloacetic acid (HAA). DBPs were linked to an increased risk of cancer. DBPs can also be quickly absorbed across the gastrointestinal tract. Hence, the presence of humic acid can cause serious health problem for living organisms.

Conventional wastewater treatment includes coagulation has some difficulties in removing the humic acid. Humic acid is hydrophobic fraction of (NOM) and it carries high charge density and a higher level of negative charge as it consists of carboxylic and phenolic groups (Tak et al., 2018). As a result, humic acid tends to dominate the colloidal charge nature of water, making it more susceptible to coagulation removal. Membrane technology is very commonly employed nowadays. Ultrafiltration and nanofiltration have been used extensively to remove humic acid, with a high proportion of the humic acid being removed. However, humic acid adds to membrane fouling, which reduces membrane function and necessitates a high-cost treatment (Yuan et al., 2000). The decrease of water quality, owing in part to NOM pollution, has resulted in more restrictive water quality laws and an increasing demand for effective water treatment technology. As a result, the Advanced Oxidation Process (AOP) can be used in wastewater treatment plants to improve humic acid removal since traditional wastewater treatment has trouble eliminating humic acid and lowering DPB levels in wastewater. AOPs are highly successful wastewater treatment technology for eliminating humic acid, which are extremely resistant to biodegradation. The AOP process produces hydroxyl radicals (OH·), which are very efficient, strong, abundant in nature, nonselective, and electrophilic, with a redox potential of 2.8V. It will degrade and mineralize them into carbon

dioxide and water. By removing a hydrogen atom from aliphatic carbon or adding a hydrogen atom to double bonds and aromatic rings, it speeds up the oxidation and breakdown of humic acid in wastewater (Kumar and Vineet, 2021).

Hence, advance oxidation process particularly ozonation is the best choice for degradation of humic acid in wastewater. Ozone is a highly oxidising agent that capable of converting organic contaminants into smaller compounds such as carbon dioxide and water. It has redox value of 2.07 V. Ozone will react with organic compounds through direct or indirect reaction. Hydroxyl radical is generated during indirect ozonation. Reaction of organic matter with ozone or hydroxyl radical, can significantly mineralize the organic compound (Gulyas et al., 1995). However, there is some limitations as ozone has low dissolution and mass transfer rate. As a result, less amount of ozone is utilized to degrade the humic acid and it will increase the demand for high ozone dosage. Thus, high cost is needed since the generation of ozone from pure oxygen will consumes high energy.

Adsorption is used with ozonation to improve the ozonation process since it is more sustainable and efficient for wastewater treatment that contains refractory organic components. According to research by (Karamah et al., 2018), ozonation alone removes 53.15 % of phenol, whereas ozonation combined with adsorption removes 78.62 %. As a result of the presence of granular activated carbon, the diffusion limitation of ozone is reduced, and the adsorption and desorption of ozone onto the adsorbent is accelerated, resulting in the transformation of ozone into active molecular radical components and the formation of hydroxyl radical. In addition, to remove heavy metals and organic debris from wastewater, a low-cost adsorbent such as lava rocks is used with ozonation in a packed column. Lava rocks have a lot of surface area, a lot of porosity, a lot of adsorption capacity, and they're cheap. The presence of lava rocks allows for a huge contact area between ozone and water, increasing gas-liquid mass transfer. As a result, the amount of ozone necessary to accomplish the appropriate humic acid elimination is