## SULIT

February 2021

## EAH221 - Fluid Mechanics for Civil Engineers

Duration : 3 hours

Please check that this examination paper consists of TWELVE (12) pages of printed material including appendix before you begin the examination.

Instructions : This paper contains SIX (6) questions. Answer FIVE (5) questions. All questions MUST BE answered on a new page.

1. (a). A manometer is used to measure the pressure between Pipe A and Pipe $B$ as shown in Figure 1. The liquid specific gravity for $S_{1}=1.5, S_{2}=0.8$ and $S_{3}=1.3$. Determine the pressure difference between Pipe $A$ and Pipe B.


Figure 1
(b). The curved face of a dam is shaped according to the equation $y=\frac{x^{2}}{12.5}$ as shown in Figure 2. For a unit width of the dam, determine the magnitude and direction of the resultant water pressure acting on the curved surface of the dam.
[12 marks]


Figure 2
2. (a). A cube of 60 cm side is submerged in a two layer fluid with specific gravity liquid $S_{1}$ and $S_{2}, 0.9$ and 1.2 respectively, as shown in Figure 3. The upper and lower halves of the cube are composed of materials with specific gravity $\mathrm{SC}_{1}$ and $\mathrm{SC}_{2}, 0.6$ and 1.4 respectively. Determine the distance of the top of the cube above the fluid interface.


Figure 3
(b). A cylindrical buoy of weight 16.5 kN with diameter 2.4 m and length 2.0 $m$ is floating with its axis vertical in sea water of specific weight $10 \mathrm{kN} / \mathrm{m}^{3}$ as shown in Figure 4. A load of 1.5 kN is placed centrally at the top of the buoy. If the buoy is in stable equilibrium, determine the maximum permissible height $h_{1}$, of. the centre of gravity of the load above the top of the buoy.


Figure 4
3. (a). A pipe with a diameter of 30 mm carries oil with specific gravity of 0.92 and velocity of $5.5 \mathrm{~m} / \mathrm{s}$. The pipe is fitted to another pipe with the radius of 20 mm . (a) Determine the velocity of the pipe at radius of 20 mm and the mass flowrate of the oil. (b) If the dynamic viscosity of oil is 9.6 x $10^{-2} \mathrm{~kg} \mathrm{~m}^{-1} \mathrm{~s}^{-1}$ flow through at the same pipe, what type of flow will occur?
[8 marks]
(b). Assuming frictionless, incompressible, one-dimensional flow of water through the series pipeline shows in Figure 5. The water flow through pipe $A B 60 \mathrm{~mm}$ in diameter and then pass through $B C$ which is 90 mm in diameter. At C the pipe forks into branch pipe $C D$ and branch pipe $C E$. The velocity at pipe $B C$ is $2.5 \mathrm{~m} / \mathrm{s}$ and volume flowrate of branch $C D$ is double than branch CE. Calculate (a) The volume flow rate for pipe AB, $B C, C D$ and CE, (b) The velocity in pipe CE, (c) The diameter of pipe CD.


Figure 5: Series Pipeline
4. (a). As shown in Figure 6, the water flows down the sloping ramp from Point 1 to Point 2 with negligible viscous efffect. Both flow are uniform at velocity at Point 1 is $0.45 \mathrm{~m} / \mathrm{s}$. At upstream depth at Point 1 is 0.25 m and the downstream depth for Point 2 can be determine by using 3 solution derived using Bernoulli dan continuity equation. However, only two solutions are realistic to calculate the value of $\mathrm{h}_{2}$ and $\mathrm{V}_{2}$. Determine these values.


Figure 6: Water flows down sloping ramp
(b). The water is flowing through a tapered pipe of diameters 15 cm and 25 cm at point $A$ and Point $B$ as shown in Figure 7. The rate of water flow through the pipe is $35 \mathrm{~L} / \mathrm{s}$. At Point A is 3.6 m above datum and at Point $B$ is 7.5 m above datum. If the pressure at Point $B$ is $86 \mathrm{~N} / \mathrm{cm}^{2}$, determine the pressure at Point $B$.


Figure 7: Section of pipe
5. (a). The principle of conservation of momentum states that the momentum of fluid in an isolated system is constant. Consider a jet of water travelling in a smooth rectangular vane at a velocity of $22.5 \mathrm{~m} / \mathrm{s}$. The rectangular section is 80 mm wide and 22.5 mm thick. The vane is attached to a rigid foundation at angle shown in Figure 8. Determine the vertical and horizontal components of the force exerted on the vane.


Figure 8
(b). Drag forces are dependent of Reynolds number in order to predict the drag forces experienced by bodies in a fluid. Consider a cylinder 80 mm diameter and 200 mm long placed in a stream of gasoline flowing at 0.5 $\mathrm{m} / \mathrm{s}$. The axis of the cylinder is normal to the direction of flow. It is given that the the temperature of gasoline is $20^{\circ} \mathrm{C}$.
(i) Calculate the drag acting on the cylinder.
(ii) Calculate the drag if the cylinder is tilted $45^{\circ}$ normal to the direction of the flow.
[10 marks]
6. (a). Broad crested weirs are robust hydraulic structures used to measure discharges in open channels. By applying Bernoulli and Froude equation, determine the expression for flow for a broad-crested weir with very low flow. The coefficient of discharge for broad crested weir is given as 0.65 .
[10 marks]
(b). A tank filled with water is connected to a multifluid manometer as shown in Figure 9. The tank is pressurised by air and is located at an altitude of 1400 m with atmospheric pressure of 83.2 kPa . Determine the air pressure in the tank if $h_{1}=0.15 \mathrm{~m}, h_{2}=0.27 \mathrm{~m}$, and $h_{3}=0.43 \mathrm{~m}$. It is given that the temperature of kerosene, mercury and water is $20^{\circ} \mathrm{C}$, respectively.
[10 marks]
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Figure 9

## APPENDIX

Table 1 - Properties of Water

## TABLE A. 1 SI units [101 kPa (abs)]

| Temperature ( ${ }^{\circ} \mathrm{C}$ ) | Specific Weight $\gamma$ $\left(\mathrm{kN} / \mathrm{m}^{3}\right)$ | Density $\stackrel{\rho}{\left(\mathrm{kg} / \mathrm{m}^{3}\right)}$ | Dynamic Viscosity $\underset{(\mathrm{Pa} \cdot \mathrm{~s})}{\boldsymbol{\eta}}$ | Kinematic Viscosity $\stackrel{\nu}{\left(\mathrm{m}^{2} / \mathrm{s}\right)}$ |
| :---: | :---: | :---: | :---: | :---: |
| 0 | 9.81 | 1000 | $1.75 \times 10^{-3}$ | $1.75 \times 10^{-6}$ |
| 5 | 9.81 | 1000 | $1.52 \times 10^{-3}$ | $1.52 \times 10^{-6}$ |
| 10 | 9.81 | 1000 | $1.30 \times 10^{-3}$ | $1.30 \times 10^{-5}$ |
| 15 | 9.81 | 1000 | $1.15 \times 10^{-3}$ | $1.15 \times 10^{-5}$ |
| 20 | 9.79 | 998 | $1.02 \times 10^{-3}$ | $1.02 \times 10^{-5}$ |
| 25 | 9.78 | 997 | $8.91 \times 10^{-4}$ | $8.94 \times 10^{-7}$ |
| 30 | 9.77 | 996 | $8.00 \times 10^{-4}$ | $8.03 \times 10^{-7}$ |
| 35 | 9.75 | 994 | $7.18 \times 10^{-4}$ | $7.22 \times 10^{-7}$ |
| 40 | 9.73 | 992 | $6.51 \times 10^{-4}$ | $6.56 \times 10^{-7}$ |
| 45 | 9.71 | 990 | $5.94 \times 10^{-4}$ | $6.00 \times 10^{-7}$ |
| 50 | 9.69 | 988 | $5.41 \times 10^{-4}$ | $5.48 \times 10^{-7}$ |
| 55 | 9.67 | 986 | $4.98 \times 10^{-4}$ | $5.05 \times 10^{-7}$ |
| 60 | 9.65 | 984 | $4.60 \times 10^{-4}$ | $4.67 \times 10^{-7}$ |
| 65 | 9.62 | 981 | $4.31 \times 10^{-4}$ | $4.39 \times 10^{-7}$ |
| 70 | 9.59 | 978 | $4.02 \times 10^{-4}$ | $4.11 \times 10^{-7}$ |
| 75 | 9.56 | 975 | $3.73 \times 10^{-4}$ | $3.83 \times 10^{-7}$ |
| 80 | 9.53 | 971 | $3.50 \times 10^{-4}$ | $3.60 \times 10^{-7}$ |
| 85 | 9.50 | 968 | $3.30 \times 10^{-4}$ | $3.41 \times 10^{-7}$ |
| 90 | 9.47 | 965 | $3.11 \times 10^{-4}$ | $3.22 \times 10^{-7}$ |
| 95 | 9.44 | 962 | $2.92 \times 10^{-4}$ | $3.04 \times 10^{-7}$ |
| 100 | 9.40 | 958 | $2.82 \times 10^{-4}$ | $2.94 \times 10^{-7}$ |

Table 2 - Physical Properties of Fluids

Physical Properties of Liquids at Standard Atmospheric Pressure 101.3 kPa , and $20^{\circ} \mathrm{C}$

| Liquid | Density <br> $\rho\left(\mathrm{kg} / \mathrm{m}^{3}\right)$ | Dynamic Viscosity <br> $\mu\left(\mathrm{N} \cdot \mathrm{s} / \mathrm{m}^{2}\right)$ | Kinematic Viscosity <br> $\nu\left(\mathrm{m}^{2} / \mathrm{s}\right)$ | Surface Tension <br> $\sigma(\mathrm{N} / \mathrm{m})$ |
| :--- | :---: | :---: | :---: | :---: |
| Ethyl alcohol | 789 | $1.19\left(10^{-3}\right)$ | $1.51\left(10^{-6}\right)$ | 0.0229 |
| Gasoline | 726 | $0.317\left(10^{-3}\right)$ | $0.437\left(10^{-6}\right)$ | 0.0221 |
| Carbon <br> tetrachloride | 1590 | $0.958\left(10^{-3}\right)$ | $0.603\left(10^{-6}\right)$ | 0.0269 |
| Kerosene | 814 | $1.92\left(10^{-3}\right)$ | $2.36\left(10^{-6}\right)$ | 0.0293 |
| Glycerin | 1260 | 1.50 | $1.19\left(10^{-3}\right)$ | 0.0633 |
| Mercury | 13550 | $1.58\left(10^{-3}\right)$ | $0.177\left(10^{-6}\right)$ | 0.466 |
| Crude oil | 880 | $30.2\left(10^{-3}\right)$ | $0.0344\left(10^{-3}\right)$ |  |

Physical Properties of Gases at Standard Atmospheric Pressure 101.3 kPa

| Gas | Density <br> $\rho\left(\mathrm{kg} / \mathrm{m}^{3}\right)$ | Dynamic Viscosity <br> $\mu\left(\mathrm{N} \cdot \mathrm{s} / \mathrm{m}^{2}\right)$ | Kinematic Viscosity <br> $\nu\left(\mathrm{m}^{2} / \mathrm{s}\right)$ | Gas Constant <br> $\mathrm{R}(\mathrm{J} /[\mathrm{kg} \cdot \mathrm{K}])$ | Specific Heat Ratio <br> $k=c_{p} / c_{v}$ |
| :--- | :---: | :---: | :---: | :---: | :---: |
| Air $\left(15^{\circ} \mathrm{C}\right)$ | 1.23 | $17.9\left(10^{-6}\right)$ | $14.6\left(10^{-6}\right)$ | 286.9 | 1.40 |
| Oxygen $\left(20^{\circ} \mathrm{C}\right)$ | 1.33 | $20.4\left(10^{-6}\right)$ | $15.2\left(10^{-6}\right)$ | 259.8 | 1.40 |
| Nitrogen $\left(20^{\circ} \mathrm{C}\right)$ | 1.16 | $17.5\left(10^{-6}\right)$ | $15.1\left(10^{-6}\right)$ | 296.8 | 1.40 |
| Hydrogen $\left(20^{\circ} \mathrm{C}\right)$ | 0.0835 | $8.74\left(10^{-6}\right)$ | $106\left(10^{-6}\right)$ | 4124 | 1.41 |
| Helium $\left(20^{\circ} \mathrm{C}\right)$ | 0.169 | $19.2\left(10^{-6}\right)$ | $114\left(10^{-6}\right)$ | 2077 | 1.66 |
| Carbon <br> dioxide $\left(20^{\circ} \mathrm{C}\right)$ | 1.84 | $14.9\left(10^{-6}\right)$ | $8.09\left(10^{-6}\right)$ | 188.9 | 1.30 |
| Methane $\left(20^{\circ} \mathrm{C}\right)$ <br> (natural gas) | 0.665 | $11.2\left(10^{-6}\right)$ | $16.8\left(10^{-6}\right)$ | 518.3 | 1.31 |


(a) $C_{D}$ vs. $N_{R}$ for lower values of $N_{R}$

(b) $C_{D}$ vs. $N_{R}$ for higher values of $N_{R}$

Figure 1 - Drag coefficients for spheres and cylinders

