
UNIVERSITI SAINS MALAYSIA

Second Semester Examination
2010/2011 Academic Session

April/May 2011

EKC 222 – Chemical Engineering Thermodynamics
[Termodinamik Kejuruteraan Kimia]

Duration : 3 hours
[Masa : 3 jam]

Please ensure that this examination paper contains SEVEN printed pages and FOUR printed page of Appendix before you begin the examination.

[Sila pastikan bahawa kertas peperiksaan ini mengandungi TUJUH muka surat yang bercetak dan EMPAT muka surat Lampiran sebelum anda memulakan peperiksaan ini.]

Instruction: Answer **ALL** questions.

Arahan: Jawab **SEMUA** soalan.]

In the event of any discrepancies, the English version shall be used.

[Sekiranya terdapat sebarang percanggahan pada soalan peperiksaan, versi Bahasa Inggeris hendaklah digunapakai].

Booklet of Thermodynamic Tables are provided.
Buku Jadual Termodinamik akan dibekalkan.

1. [a] Answer the following questions in your own words:
Jawab soalan-soalan berikut dengan perkataan anda sendiri:
- [i] As a consequence of thermal equilibrium, Zeroth Law of Thermodynamics can be defined and it serves as the working principle for thermometer. Explain why a piece of ice will melt in a glass of water under the context of Zeroth Law.
- Lanjutan dari keseimbangan terma, Hukum Termodinamik Sifar boleh ditakrifkan dan berfungsi sebagai prinsip kerja untuk termometer. Jelaskan mengapa seketul ais akan cair dalam segelas air di bawah Hukum Termodinamik Sifar.*
- [2 marks/markah]
- [ii] According to the 1st Law of Thermodynamics energy is always conserved. However, for exothermic reaction, energy is released to the surrounding. Explain why exothermic reaction is not violating the 1st Law.
- Menurut Hukum Termodinamik Pertama, tenaga selalunya diabadikan. Walau bagaimanapun, untuk tindak balas eksotermik, tenaga dilepaskan ke persekitaran. Jelaskan mengapa tindak balas eksotermik tidak melanggar Hukum Termodinamik Pertama.*
- [2 marks/markah]
- [iii] According to Clausius statement of 2nd Law of Thermodynamics, the entropy of the universe tends to a maximum. Explain why this statement leads to the impossibility of perpetual motion machine.
- Menurut kenyataan Clausius, bagi Hukum Termodinamik Kedua, entropi alam sekitar cenderung ke arah maksimum. Jelaskan mengapa kenyataan ini menjurus kepada ketidakmungkinan mesin gerak abadi.*
- [2 marks/markah]
- [b] For an ideal gas with constant heat capacities, show that
Untuk gas unggul dengan muatan haba malar, tunjukkan:
- [i] For a temperature change from T_1 to T_2 , ΔS of the gas is greater when the change occurs at constant pressure than when it occurs at constant volume.
- Bagi pertukaran suhu dari T_1 ke T_2 , ΔS untuk gas ini mengalami perubahan lebih besar pada tekanan malar berbanding perubahan pada isipadu malar.*

- [ii] For a pressure change from P_1 to P_2 , the sign of ΔS for an isothermal changes is opposite that for a constant volume change.

Bagi pertukaran tekanan dari P_1 ke P_2 , tanda untuk ΔS bagi perubahan sesuhu adalah bertentangan dengan perubahan pada isipadu malar.

Hint:

Petunjuk:

$$\Delta S = C_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{P_2}{P_1}\right)$$

[8 marks/markah]

- [c] Steam enters a nozzle at 4 MPa and 640 °C with velocity of 20 m/s. This process may be considered reversible and adiabatic. The nozzle exit pressure is 0.1 MPa.

Stim memasuki muncung pada 4 MPa dan 640 °C dengan kelajuan 20 m/s. Proses ini adalah proses berbalik dan adiabatik. Tekanan keluaran muncung ini ialah 0.1 MPa.

- [i] Draw a sketch of this process. Include all known information.
Lukiskan satu gambar rajah dengan semua informasi yang dibekalkan untuk mewakili proses ini.
- [ii] What is the entropy change of the stream?
Apakah perubahan entropi untuk arus ini?
- [iii] What is the exit temperature?
Apakah suhu keluaran?
- [iv] What is the exit velocity?
Apakah kelajuan keluaran?

[11 marks/markah]

2. [a] Briefly explain the phase change from point 1 to point 4 using Figure Q.2.[a].
 Terangkan dengan ringkas perubahan fasa dari titik 1 ke titik 4 menggunakan Rajah S.2.[a].

[3 marks/markah]

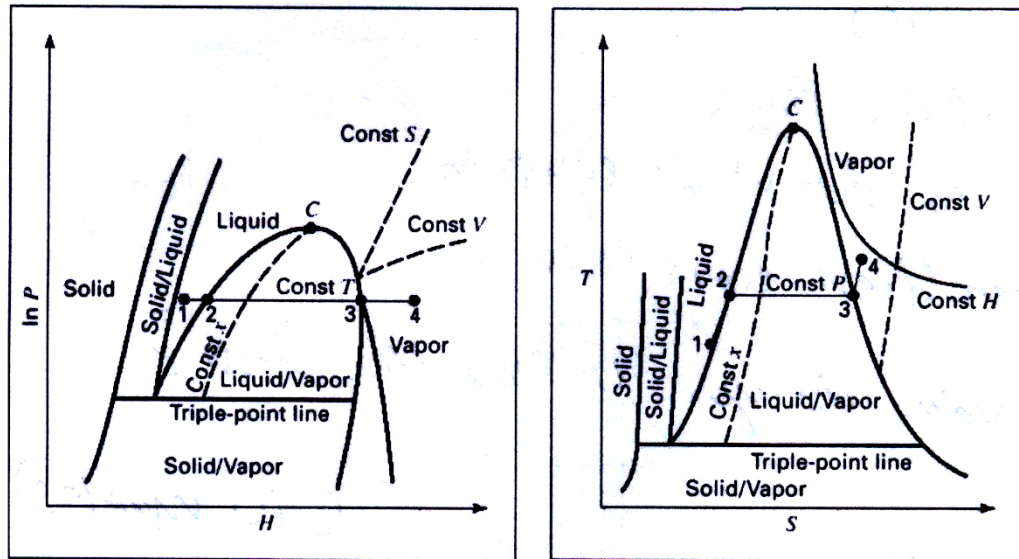


Figure Q.2.[a]
 Rajah S.2.[a]

- [b] What is the difference between
 Apakah perbezaan antara
- [i] a refrigerator and a heat pump
 peti sejuk dan pam haba
 - [ii] a refrigerator and an air conditioner
 peti sejuk dan penyaman udara

[2 marks/markah]

- [c] Air enters the compressor of an ideal gas refrigeration cycle at 12°C and 50 kPa and the turbine at 47°C and 250 kPa. The mass flow rate of air through the cycle is 0.08 kg/s. Assuming variable specific heat for air, determine

Udara memasuki pemampat suatu kitar penyejuk gas unggul pada 12°C dan 50 kPa dan sebuah turbin pada 47°C dan 250 kPa. Kadar aliran jisim udara melalui kitaran ialah 0.08 kg/s. Andaikan haba tentu bagi udara berubah, kirakan

- [i] the rate of refrigeration
 kadar penyejukan
- [ii] the net power input, and
 masukan kuasa bersih, dan
- [iii] the coefficient of performance
 pekali prestasi

[10 marks/markah]

...5/-

[d] Calculate the fugacity of water at 647 K and 114 atm using
Kirakan fugasiti air pada 647 K dan 114 atm menggunakan

- [i] the steam table
jadual stim
- [ii] the van der Waals equation
persamaan van der Waals
- [iii] generalized correlation
sekaitan umum

Which value do you believe the most? Justify.

Nilai manakah yang anda paling percaya? Wajarkan jawapan anda.

[10 marks/markah]

3. [a] In his book *The Trouble Waters*, Henry Morris an American young earth creationist proclaims:

Dalam bukunya "The Trouble Waters", Henry Morris seorang pemuda Amerika yang mempercayai penciptaan bumi menyatakan:

"The Law of increasing entropy is an impenetrable barrier which no evolutionary mechanism yet suggested has ever been able to overcome. Evolution and entropy are opposing and mutually exclusive concepts. If the entropy principle is really a universal law, then evolution must be impossible."

"Hukum termodinamik tentang peningkatan entropi merupakan sekatan tak terbatas yang bertentangan dengan mekanisma evolusi. Evolusi dan entropi adalah dua konsep yang bertentangan dan tidak bersetujui di antara satu sama lain. Jika prinsip entropi adalah suatu hukum universal yang benar, maka evolusi mestilah mustahil."

Is this argument scientifically sound? Explain.

Adakah hujah ini saintifik? Jelaskan.

[5 marks/markah]

[b] Calculate the change in entropy when 1 mol of water is heated from 250 K to 290 K, given that the molar heat capacities at constant pressure $(C_p)_{\text{ice}} = 2.09 + 0.126T$ [J/K] and $(C_p)_{\text{water}} = 75.3$ J/K and the heat of melting $(\Delta H)_m = 6000$ J/mol. (Hint: Melting point of water at 273 K, hence, the water is undergoing phase transition).

Kirakan perubahan entropi apabila 1 mol air dipanaskan dari 250 K ke 290 K. Diberi muatan haba pada tekanan malar $(C_p)_{\text{ais}} = 2.09 + 0.126T$ [J/K] dan $(C_p)_{\text{air}} = 75.3$ [J/K] dengan tenaga haba pencairan $(\Delta H)_m = 6000$ J/mol. (Petunjuk: Suhu pencairan air ialah 273 K, justeru air mengalami perubahan fasa).

Given: $\Delta H = nC_p dT$

Diberi:

[6 marks/markah]

...6/-

- [c] The equation of state of a van der Waals gas is given by
Persamaan keadaan untuk gas van der Waals diberikan sebagai

$$\left(P + \frac{a}{V^2}\right)(V - b) = RT \quad \text{Equation 3.1}$$

Persamaan 3.1

Derive mathematical expressions for W , ΔU , Q and ΔH of this gas for an isothermal reversible expansion from an initial volume V_1 to final volume V_2 .
 (Hint: $[\partial U / \partial V]_T = a/V^2$)

*Terbitkan perhubungan matematik untuk W , ΔU , Q dan ΔH untuk gas ini yang mengalami perkembangan berbalik sesuhu dari isipadu V_1 kepada V_2 .
 (Petunjuk: $[\partial U / \partial V]_T = a/V^2$)*

[14 marks/markah]

4. [a] Briefly explain the use of the following equipments:
Terangkan dengan ringkas kegunaan peralatan di bawah:

- [i] Turbine
Turbin
- [ii] Compressor
Pemampat
- [iii] Throttle valve
Injap pendikit
- [iv] Expander
Pengembang
- [v] Condenser
Pemeluwap
- [vi] Evaporator
Penyejat

[6 marks/markah]

- [b] Figure Q.4.[b] is a plot of the natural log of the activity coefficient ($\ln \gamma_i$) of a binary liquid mixture of species a and b vs. mole fraction of species a (x_a) at 300K.

Rajah S.4.[b] ialah plot log asli pekali aktiviti ($\ln \gamma_i$) bagi satu campuran cecair binari a dan b melawan pecahan mol spesis a (x_a) pada 300K.

- [i] What is the reference state for each species?
Apakah keadaan rujukan untuk setiap sepsis?
- [ii] Show that the Gibbs-Duhem equation is satisfied at $x_a = 0.6$.
Tunjukkan bahawa persamaan Gibbs-Duhem dipatuhi pada $x_a = 0.6$.

...7/-

- [iii] Come up with an appropriate model for g^E for this system and find the value of the model parameters.

Terbitkan model yang sesuai untuk g^E bagi sistem ini, dan dapatkan nilai untuk parameter model.

- [iv] Is it possible for species a and b to separate into two liquid phase? Explain.

Mungkinkah spesis a dan b dipisahkan kepada dua fasa cecair? Terangkan.

[19 marks/markah]

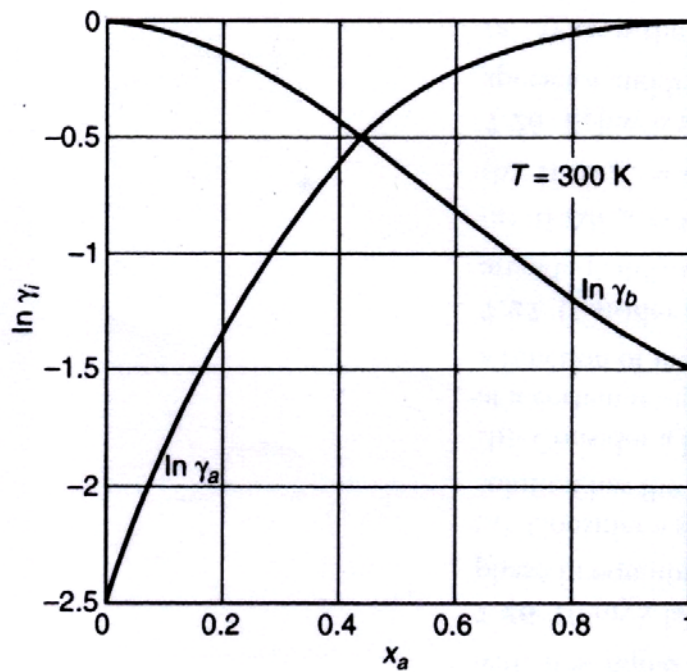


Figure Q.4.[b].
Rajah S.4.[b].

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Appendix

Table A.2: Values of the Universal Gas Constant

$$\begin{aligned}
 R &= 8.314 \text{ J mol}^{-1} \text{ K}^{-1} = 8.314 \text{ m}^3 \text{ Pa mol}^{-1} \text{ K}^{-1} \\
 &= 83.14 \text{ cm}^3 \text{ bar mol}^{-1} \text{ K}^{-1} = 8,314 \text{ cm}^3 \text{ kPa mol}^{-1} \text{ K}^{-1} \\
 &= 82.06 \text{ cm}^3(\text{atm}) \text{ mol}^{-1} \text{ K}^{-1} = 62,356 \text{ cm}^3(\text{torr}) \text{ mol}^{-1} \text{ K}^{-1} \\
 &= 1.987(\text{cal}) \text{ mol}^{-1} \text{ K}^{-1} = 1.986(\text{Btu})(\text{lb mole})^{-1}(\text{R})^{-1} \\
 &= 0.7302(\text{ft})^3(\text{atm})(\text{lb mol})^{-1}(\text{R})^{-1} = 10.73(\text{ft})^3(\text{psia})(\text{lb mol})^{-1}(\text{R})^{-1} \\
 &= 1,545(\text{ft})(\text{lb}_f)(\text{lb mol})^{-1}(\text{R})^{-1}
 \end{aligned}$$

(H [=] kJ/kg, S [=] kJ/kgK)

Table F.2. Superheated Steam, SI Units (Continued)

P/kPa ($t^{\text{sat}}/^\circ\text{C}$)		sat. liq.	sat. vap.	TEMPERATURE: t °C (TEMPERATURE: T kelvins)							
				425 (698.15)	450 (723.15)	475 (748.15)	500 (773.15)	525 (798.15)	550 (823.15)	600 (873.15)	650 (923.15)
2400 (221.78)	V	1.193	83.199	130.44	135.61	140.73	145.82	150.88	155.91	165.92	175.86
	U	949.066	2600.7	2984.5	3027.1	3069.9	3112.9	3156.1	3199.6	3287.7	3377.2
	H	951.929	2800.4	3297.5	3352.6	3407.7	3462.9	3518.2	3573.8	3685.9	3799.3
	S	2.5343	6.2690	7.1189	7.1964	7.2713	7.3439	7.4144	7.4830	7.6152	7.7414
2500 (223.94)	V	1.197	79.905	125.07	130.04	134.97	139.87	144.74	149.58	159.21	168.76
	U	958.969	2601.2	2983.4	3026.2	3069.0	3112.1	3155.4	3198.9	3287.1	3376.7
	H	961.962	2800.9	3296.1	3351.3	3406.5	3461.7	3517.2	3572.9	3685.1	3798.6
	S	2.5543	6.2536	7.0986	7.1763	7.2513	7.3240	7.3946	7.4633	7.5956	7.7220
2600 (226.04)	V	1.201	76.856	120.11	124.91	129.66	134.38	139.07	143.74	153.01	162.21
	U	968.597	2601.5	2982.3	3025.2	3068.1	3111.2	3154.6	3198.2	3286.5	3376.1
	H	971.720	2801.4	3294.6	3349.9	3405.3	3460.6	3516.2	3571.9	3684.3	3797.9
	S	2.5736	6.2387	7.0789	7.1568	7.2320	7.3048	7.3755	7.4443	7.5768	7.7033
2700 (228.07)	V	1.205	74.025	115.52	120.15	124.74	129.30	133.82	138.33	147.27	156.14
	U	977.968	2601.8	2981.2	3024.2	3067.2	3110.4	3153.8	3197.5	3285.8	3375.6
	H	981.222	2801.7	3293.1	3348.6	3404.0	3459.5	3515.2	3571.0	3683.5	3797.1
	S	2.5924	6.2244	7.0600	7.1381	7.2134	7.2863	7.3571	7.4260	7.5587	7.6853
2800 (230.05)	V	1.209	71.389	111.25	115.74	120.17	124.58	128.95	133.30	141.94	150.50
	U	987.100	2602.1	2980.2	3023.2	3066.3	3109.6	3153.1	3196.8	3285.2	3375.0
	H	990.485	2802.0	3291.7	3347.3	3402.8	3458.4	3514.1	3570.0	3682.6	3796.4
	S	2.6106	6.2104	7.0416	7.1199	7.1954	7.2685	7.3394	7.4084	7.5412	7.6679
2900 (231.97)	V	1.213	68.928	107.28	111.62	115.92	120.18	124.42	128.62	136.97	145.26
	U	996.008	2602.3	2979.1	3022.3	3065.5	3108.8	3152.3	3196.1	3284.6	3374.5
	H	999.524	2802.2	3290.2	3346.0	3401.6	3457.3	3513.1	3569.1	3681.8	3795.7
	S	2.6283	6.1969	7.0239	7.1024	7.1780	7.2512	7.3222	7.3913	7.5243	7.6511
3000 (233.84)	V	1.216	66.626	103.58	107.79	111.95	116.08	120.18	124.26	132.34	140.36
	U	1004.7	2602.4	2978.0	3021.3	3064.6	3107.9	3151.5	3195.4	3284.0	3373.9
	H	1008.4	2802.3	3288.7	3344.6	3400.4	3456.2	3512.1	3568.1	3681.0	3795.0
	S	2.6455	6.1837	7.0067	7.0854	7.1612	7.2345	7.3056	7.3748	7.5079	7.6349
3100 (235.67)	V	1.220	64.467	100.11	104.20	108.24	112.24	116.22	120.17	128.01	135.78
	U	1013.2	2602.5	2976.9	3020.3	3063.7	3107.1	3150.8	3194.7	3283.3	3373.4
	H	1017.0	2802.3	3287.3	3343.3	3399.2	3455.1	3511.0	3567.2	3680.2	3794.3
	S	2.6623	6.1709	6.9900	7.0689	7.1448	7.2183	7.2895	7.3588	7.4920	7.6191

	V	1.224	62.439	96.859	100.83	104.76	108.65	112.51	116.34	123.95	131.48
3200	U	1021.5	2602.5	2975.9	3019.3	3062.8	3106.3	3150.0	3193.9	3282.7	3372.8
(237.45)	H	1025.4	2802.3	3285.8	3342.0	3398.0	3454.0	3510.0	3566.2	3679.3	3793.6
	S	2.6786	6.1585	6.9738	7.0528	7.1290	7.2026	7.2739	7.3433	7.4767	7.6039
	V	1.227	60.529	93.805	97.668	101.49	105.27	109.02	112.74	120.13	127.45
3300	U	1029.7	2602.5	2974.8	3018.3	3061.9	3105.5	3149.2	3193.2	3281.5	3371.3
(239.18)	H	1033.7	2802.3	3284.3	3340.6	3396.8	3452.8	3509.0	3565.3	3678.5	3792.9
	S	2.6945	6.1463	6.9580	7.0373	7.1136	7.1873	7.2588	7.3282	7.4618	7.5891
	V	1.231	58.728	90.930	94.692	98.408	102.09	105.74	109.36	116.54	123.65
3400	U	1037.6	2602.5	2973.7	3017.4	3061.0	3104.6	3148.4	3192.5	3281.5	3371.7
(240.88)	H	1041.8	2802.1	3282.8	3339.3	3395.5	3451.7	3507.9	3564.3	3677.7	3792.1
	S	2.7101	6.1344	6.9426	7.0221	7.0986	7.1724	7.2440	7.3136	7.4473	7.5747
	V	1.235	57.025	88.220	91.886	95.505	99.088	102.64	106.17	113.15	120.07
3500	U	1045.4	2602.4	2972.6	3016.4	3060.1	3103.8	3147.7	3191.8	3280.8	3371.2
(242.54)	H	1049.8	2802.0	3281.3	3338.0	3394.3	3450.6	3506.9	3563.4	3676.9	3791.4
	S	2.7253	6.1228	6.9277	7.0074	7.0840	7.1580	7.2297	7.2993	7.4332	7.5607
	V	1.238	55.415	85.660	89.236	92.764	96.255	99.716	103.15	109.96	116.69
3600	U	1053.1	2602.2	2971.5	3015.4	3059.2	3103.0	3146.9	3191.1	3280.2	3370.6
(244.16)	H	1057.6	2801.7	3279.8	3336.6	3393.1	3449.5	3505.9	3562.4	3676.1	3790.7
	S	2.7401	6.1115	6.9131	6.9930	7.0698	7.1439	7.2157	7.2854	7.4195	7.5471
	V	1.242	53.888	83.238	86.728	90.171	93.576	96.950	100.30	106.93	113.49
3700	U	1060.6	2602.1	2970.4	3014.4	3058.2	3102.1	3146.1	3190.4	3279.6	3370.1
(245.75)	H	1065.2	2801.4	3278.4	3335.3	3391.9	3448.4	3504.9	3561.5	3675.2	3790.0
	S	2.7547	6.1004	6.8989	6.9790	7.0559	7.1302	7.2021	7.2719	7.4061	7.5339
	V	1.245	52.438	80.944	84.353	87.714	91.038	94.330	97.596	104.06	110.46
3800	U	1068.0	2601.9	2969.3	3013.4	3057.3	3101.3	3145.4	3189.6	3279.0	3369.5
(247.31)	H	1072.7	2801.1	3276.8	3333.9	3390.7	3447.2	3503.8	3560.5	3674.4	3789.3
	S	2.7689	6.0896	6.8849	6.9653	7.0424	7.1168	7.1888	7.2587	7.3931	7.5210
	V	1.249	51.061	78.767	82.099	85.383	88.629	91.844	95.033	101.35	107.59
3900	U	1075.3	2601.6	2968.2	3012.4	3056.4	3100.5	3144.6	3188.9	3278.3	3369.0
(248.84)	H	1080.1	2800.8	3275.3	3332.6	3389.4	3446.1	3502.8	3559.5	3673.6	3788.6
	S	2.7828	6.0789	6.8713	6.9519	7.0292	7.1037	7.1759	7.2459	7.3804	7.5084
	V	1.252	49.749	76.698	79.958	83.169	86.341	89.483	92.598	98.763	104.86
4000	U	1082.4	2601.3	2967.0	3011.4	3055.5	3099.6	3143.8	3188.2	3277.7	3368.4
(250.33)	H	1087.4	2800.3	3273.8	3331.2	3388.2	3445.0	3501.7	3558.6	3672.8	3787.9
	S	2.7965	6.0685	6.8581	6.9388	7.0163	7.0909	7.1632	7.2333	7.3680	7.4961

Table F.2: Superheated Steam, SI Units

		TEMPERATURE: t °C (TEMPERATURE: T kelvins)									
		sat. liq.	sat. vap.	75 (348.15)	100 (373.15)	125 (398.15)	150 (423.15)	175 (448.15)	200 (473.15)	225 (498.15)	250 (523.15)
1 (6.98)	V	1.000	129200.	160640.	172180.	183720.	195270.	206810.	218350.	229890.	241430.
	U	29.334	2385.2	2480.8	2516.4	2552.3	2588.5	2624.9	2661.7	2698.8	2736.3
	H	29.335	2514.4	2641.5	2688.6	2736.0	2783.7	2831.7	2880.1	2928.7	2977.7
10 (45.83)	S	0.1060	8.9767	9.3828	9.5136	9.6365	9.7527	9.8629	9.9679	10.0681	10.1641
	V	1.010	14670.	16030.	17190.	18350.	19510.	20660.	21820.	22980.	24130.
	U	191.822	2438.0	2479.7	2515.6	2551.6	2588.0	2624.5	2661.4	2698.6	2736.1
20 (60.09)	H	191.832	2584.8	2640.0	2687.5	2735.2	2783.1	2831.2	2879.6	2928.4	2977.4
	S	0.6493	8.1511	8.3168	8.4486	8.5722	8.6888	8.7994	8.9045	9.0049	9.1010
	V	1.017	7649.8	8000.0	8584.7	9167.1	9748.0	10320.	10900.	11480.	12060.
30 (69.12)	U	251.432	2456.9	2478.4	2514.6	2550.9	2587.4	2624.1	2661.0	2698.3	2735.8
	H	251.453	2609.9	2638.4	2686.3	2734.2	2782.3	2830.6	2879.2	2928.0	2977.1
	S	0.8321	7.9094	7.9933	8.1261	8.2504	8.3676	8.4785	8.5839	8.6844	8.7806
40 (75.89)	V	1.022	5229.3	5322.0	5714.4	6104.6	6493.2	6880.8	7267.5	7653.8	8039.7
	U	289.271	2468.6	2477.1	2513.6	2550.2	2586.8	2623.6	2660.7	2698.0	2735.6
	H	289.302	2625.4	2636.8	2685.1	2733.3	2781.6	2830.0	2878.7	2927.6	2976.8
50 (81.35)	S	0.9441	7.7695	7.8024	7.9363	8.0614	8.1791	8.2903	8.3960	8.4967	8.5930
	V	1.027	3993.4	4279.2	4573.3	4865.8	5157.2	5447.8	5738.0	6027.7
	U	317.609	2477.1	2512.6	2549.4	2586.2	2623.2	2660.3	2697.7	2735.4
75 (91.79)	H	317.650	2636.9	2683.8	2732.3	2780.9	2829.5	2878.2	2927.2	2976.5
	S	1.0261	7.6709	7.8009	7.9268	8.0450	8.1566	8.2624	8.3633	8.4598
	V	1.030	3240.2	3418.1	3654.5	3889.3	4123.0	4356.0	4588.5	4820.5
100 (99.63)	U	340.513	2484.0	2511.7	2548.6	2585.6	2622.7	2659.9	2697.4	2735.1
	H	340.564	2646.0	2682.6	2731.4	2780.1	2828.9	2877.7	2926.8	2976.1
	S	1.0912	7.5947	7.6953	7.8219	7.9406	8.0526	8.1587	8.2598	8.3564
150 (99.63)	V	1.037	2216.9	2269.8	2429.4	2587.3	2744.2	2900.2	3055.8	3210.9
	U	384.374	2496.7	2509.2	2546.7	2584.2	2621.6	2659.0	2696.7	2734.5
	H	384.451	2663.0	2679.4	2728.9	2778.2	2827.4	2876.6	2925.8	2975.3
200 (99.63)	S	1.2131	7.4570	7.5014	7.6300	7.7500	7.8629	7.9697	8.0712	8.1681
	V	1.043	1693.7	1695.5	1816.7	1936.3	2054.7	2172.3	2289.4	2406.1
	U	417.406	2506.1	2506.6	2544.8	2582.7	2620.4	2658.1	2695.9	2733.9
250 (99.63)	H	417.511	2675.4	2676.2	2726.5	2776.3	2825.9	2875.4	2924.9	2974.5
	S	1.3027	7.3598	7.3618	7.4923	7.6137	7.7275	7.8349	7.9369	8.0342

Table F.2. Superheated Steam, SI Units (Continued)

P/kPa ($t^{\text{sat}} / ^\circ\text{C}$)	sat. liq.	sat. vap.	TEMPERATURE: t °C (TEMPERATURE: T kelvins)								
			300 (573.15)	350 (623.15)	400 (673.15)	450 (723.15)	500 (773.15)	550 (823.15)	600 (873.15)	650 (923.15)	
1 (6.98)	V	1.000	129200.	264500.	287580.	310660.	333730.	356810.	379880.	402960.	426040.
	U	29.334	2385.2	2812.3	2889.9	2969.1	3049.9	3132.4	3216.7	3302.6	3390.3
	H	29.335	2514.4	3076.8	3177.5	3279.7	3383.6	3489.2	3596.5	3705.6	3816.4
	S	0.1060	8.9767	10.3450	10.5133	10.6711	10.8200	10.9612	11.0957	11.2243	11.3476
10 (45.83)	V	1.010	14670.	26440.	28750.	31060.	33370.	35670.	37980.	40290.	42600.
	U	191.822	2438.0	2812.2	2889.8	2969.0	3049.8	3132.3	3216.6	3302.6	3390.3
	H	191.832	2584.8	3076.6	3177.3	3279.6	3383.5	3489.1	3596.5	3705.5	3816.3
	S	0.6493	8.1511	9.2820	9.4504	9.6083	9.7572	9.8984	10.0329	10.1616	10.2849
20 (60.09)	V	1.017	7649.8	13210.	14370.	15520.	16680.	17830.	18990.	20140.	21300.
	U	251.432	2456.9	2812.0	2889.6	2968.9	3049.7	3132.3	3216.5	3302.5	3390.2
	H	251.453	2609.9	3076.4	3177.1	3279.4	3383.4	3489.0	3596.4	3705.4	3816.2
	S	0.8321	7.9094	8.9618	9.1303	9.2882	9.4372	9.5784	9.7130	9.8416	9.9650
30 (69.12)	V	1.022	5229.3	8810.8	9581.2	10350.	11120.	11890.	12660.	13430.	14190.
	U	289.271	2468.6	2811.8	2889.5	2968.7	3049.6	3132.2	3216.5	3302.5	3390.2
	H	289.302	2625.4	3076.1	3176.9	3279.3	3383.3	3488.9	3596.3	3705.4	3816.2
	S	0.9441	7.7695	8.7744	8.9430	9.1010	9.2499	9.3912	9.5257	9.6544	9.7778
40 (75.89)	V	1.027	3993.4	6606.5	7184.6	7762.5	8340.1	8917.6	9494.9	10070.	10640.
	U	317.609	2477.1	2811.6	2889.4	2968.6	3049.5	3132.1	3216.4	3302.4	3390.1
	H	317.650	2636.9	3075.9	3176.8	3279.1	3383.1	3488.8	3596.2	3705.3	3816.1
	S	1.0261	7.6709	8.6413	8.8100	8.9680	9.1170	9.2583	9.3929	9.5216	9.6450
50 (81.35)	V	1.030	3240.2	5283.9	5746.7	6209.1	6671.4	7133.5	7595.5	8057.4	8519.2
	U	340.513	2484.0	2811.5	2889.2	2968.5	3049.4	3132.0	3216.3	3302.3	3390.1
	H	340.564	2646.0	3075.7	3176.6	3279.0	3383.0	3488.7	3596.1	3705.2	3816.0
	S	1.0912	7.5947	8.5380	8.7068	8.8649	9.0139	9.1552	9.2898	9.4185	9.5419
75 (91.79)	V	1.037	2216.9	3520.5	3829.4	4138.0	4446.4	4754.7	5062.8	5370.9	5678.9
	U	384.374	2496.7	2811.0	2888.9	2968.2	3049.2	3131.8	3216.1	3302.2	3389.9
	H	384.451	2663.0	3075.1	3176.1	3278.6	3382.7	3488.4	3595.8	3705.0	3815.9
	S	1.2131	7.4570	8.3502	8.5191	8.6773	8.8265	8.9678	9.1025	9.2312	9.3546
100 (99.63)	V	1.043	1693.7	2638.7	2870.8	3102.5	3334.0	3565.3	3796.5	4027.7	4258.8
	U	417.406	2506.1	2810.6	2888.6	2968.0	3049.0	3131.6	3216.0	3302.0	3389.8
	H	417.511	2675.4	3074.5	3175.6	3278.2	3382.4	3488.1	3595.6	3704.8	3815.7
	S	1.3027	7.3598	8.2166	8.3858	8.5442	8.6934	8.8348	8.9695	9.0982	9.2217